

2nd International Conference on Sustainable Solid Waste

Management

12- 14 June, 2014 - Athens, Greece

The effect of acid pretreatment on bio-ethanol and bio-hydrogen production from sunflower straw

G. Antonopoulou¹, G. Dimitrellos¹, D. Vayenas^{1,2} and G. Lyberatos^{1,3}



¹ Institute of Chemical Engineering Sciences, Stadiou 1, Platani, Patras, 26504, Greece

² Department of Environmental and Natural Resources Management, University of Patras, 2 G. Seferi st, Agrinio, GR30100, Greece

³ School of Chemical Engineering, National Technical University of Athens, GR 15780 Athens, Greece

Sunflower straw (SS)

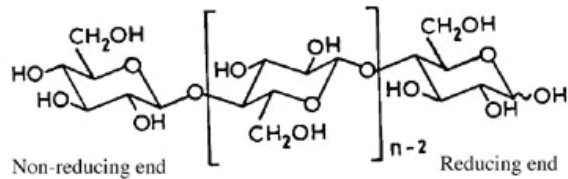


- ☀ Sunflower is the fourth oil-seed source worldwide with more than 25 million hectares cultivated land surface
- ☀ Sunflower has a high-lipid content seed and represents an important resource for biodiesel production.
- ☀ While it is mainly harvested for its oil, the remainder of the plant, such as the straw, remains to a large extent unutilized.
- ☀ Each hectare of sunflower culture could produce 3-7tons of dry biomass, including heads and stalks (*Marechal and Rigal, 1999*)
- ☀ In order to maintain a competitive advantage in the world market and ensure a sustained economic return in the production of this oil crop, the potential of conversion of this **lignocellulosic residue** in bioenergy should be explored and exploited.

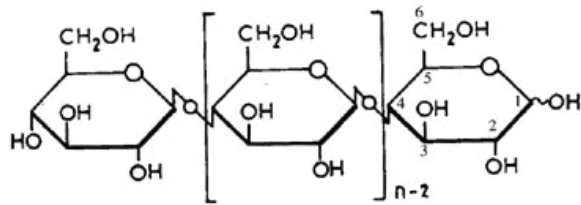




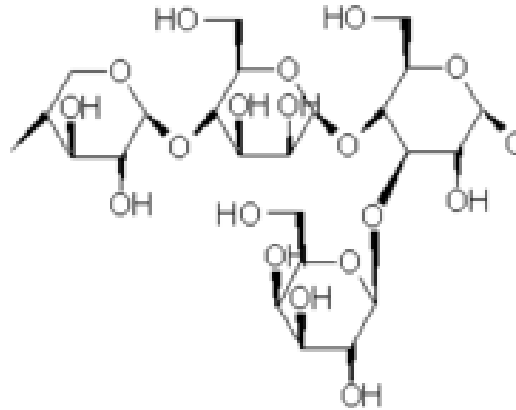
Lignocellulosic biomass



Sometimes shown as

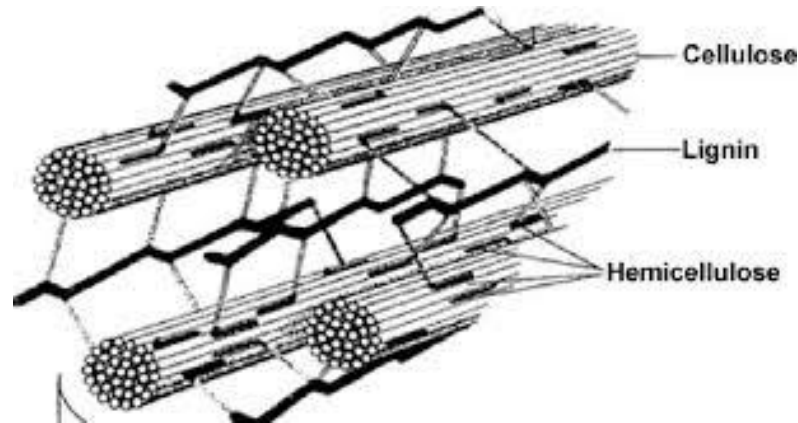
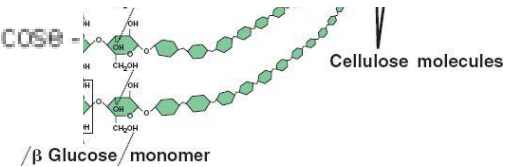
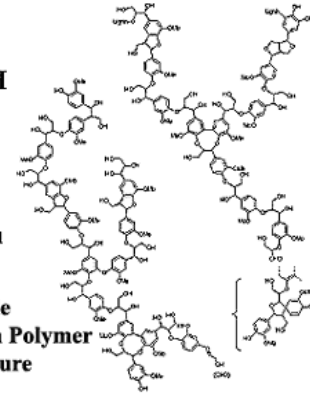
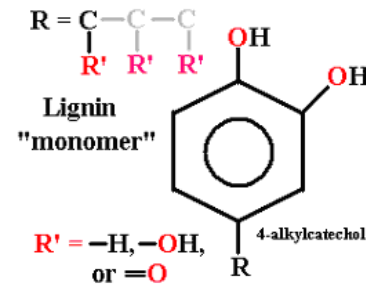


Cellulose

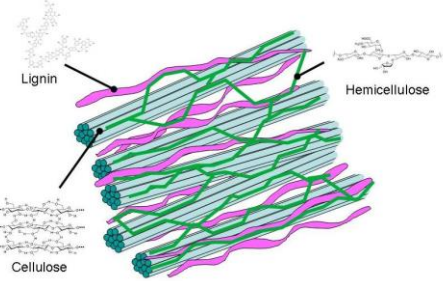


- Xylose - $\beta(1,4)$ - Mannose - $\beta(1,4)$ - Glucose -
- $\alpha(1,3)$ - Galactose

Hemicellulose

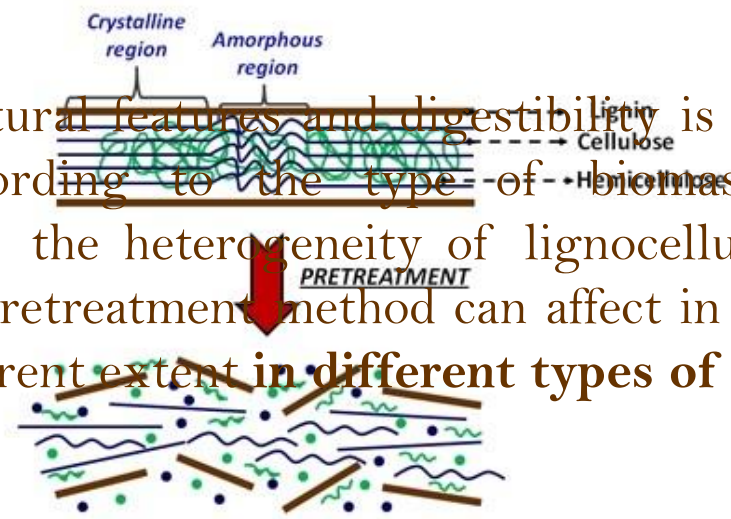


Pretreatment



☀ Pretreatment is commonly accepted to be an essential prerequisite to make lignocellulosic biomass accessible to enzymatic attack, by breaking the lignin seal, removing hemicellulose, or disrupting the crystalline structure of cellulose (*Fan et al., 1981*)

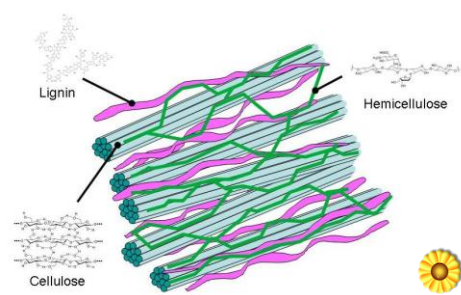
☀ The correlation of structural features and digestibility is reported to be of variant importance according to the type of biomass to be treated. Consequently, because of the heterogeneity of lignocellulosic biomass the application of the same pretreatment method can affect in a different degree and have an effect of different extent in different types of biomass.



Best pretreatment method for intended bioconversion



Pretreatment



☀ A variety of pretreatment including mechanical, thermochemical or thermal processes, have been developed for changing the chemical and structural composition of biomass and improving the enzymatic conversion efficiency (*Hendriks and Zeeman, 2009*).

☀ Acid pretreatment, has been proposed as an efficient pretreatment method for ethanol or fermentative hydrogen production (*Schell et al., 2003; Sanchez et al., 2004; Garcia et al., 2014*)

☀ During acid pretreatment, hemicellulosic fraction of biomass is hydrolyzed to soluble sugars and compounds such as furfural and/or hydroxymethylfurfural (HMF), formic and acetic acids can also be observed (*Ramos, 2003*).

☀ These compounds might have an inhibitory or toxic effect on bacteria or yeasts that are used in subsequent bioconversions.

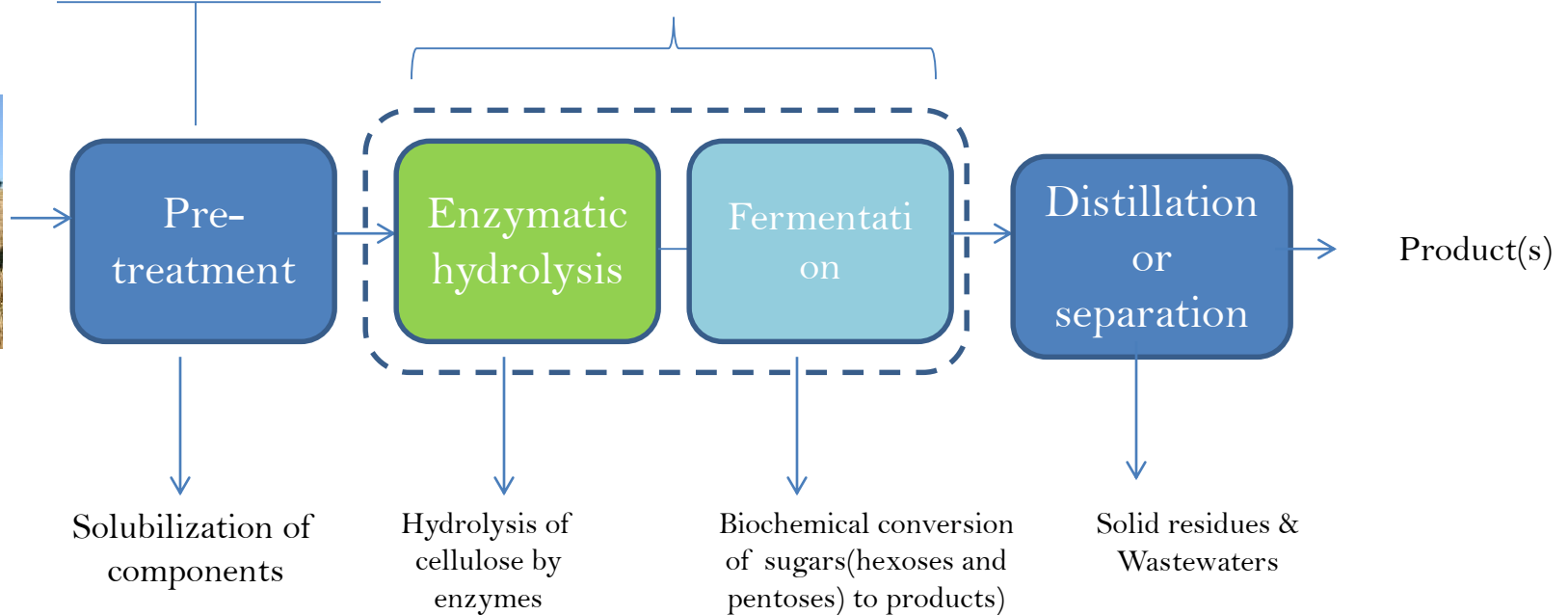


Biochemical processing



Physical, chemical
or biological
pretreatment

Simultaneous or separate
saccharification and fermentation



✓ Cost efficient production of sugars from biomass is a key pre-requisite for any biorefinery based on sugar route.



The process followed....



Acid Pre-treatment

Solubilization of hemicellulose

Simultaneous saccharification and fermentation (SSF)

Chemical agent	Concentration (g/100gTS)	Conditions
H ₂ SO ₄	2, 10, 20	1h, 120°C
H ₃ PO ₄	2, 10, 20	1h, 120°C
HCl	2, 10, 20	1h, 120°C
no chemical	thermal	1h, 120°C

Hydrolysis of cellulose by enzymes

Biochemical conversion of sugars(hexoses and pentoses) to products)

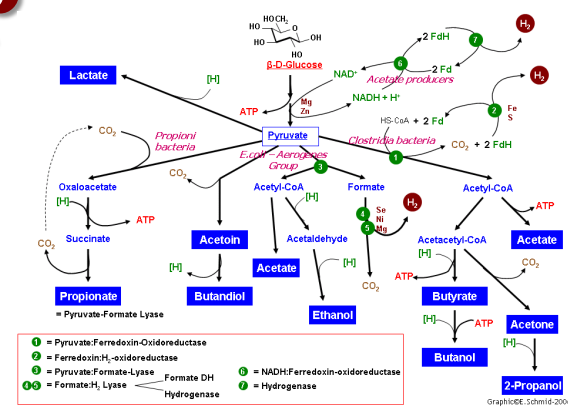
Ethanol

Hydrogen

☀ For all pretreatment methods: mass ratio of solid(g) to liquid(mL) was 5:100 (organic load 5% w/v)



Why hydrogen?



- ☀️ A clean and environmentally friendly fuel which produces water instead of greenhouse gases, when combusted
- ☀️ Possesses a high-energy yield (122 kJ/g)
- ☀️ Could be directly used to produce electricity through fuel cells
- ☀️ Can be produced by renewable raw materials, such as wastes / wastewaters and energy crops through biological processes



Fermentative hydrogen production

Acetic acid production



Butyric acid production



Propionic acid production



Lactate production



Ethanol production



Mixed acid fermentations



lower yields of H_2

✓ The absence or presence of hydrogen-consuming microorganisms in the microbial consortium also affects the microbial metabolic balance

✓ Mixed cultures need to be pretreated in order to suppress hydrogen-consuming bacterial activity while still preserving the activity of the hydrogen-producing bacteria



Heat treatment (100°C, 15min)



Bioethanol production

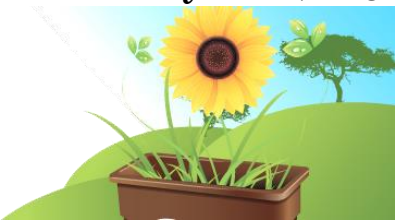
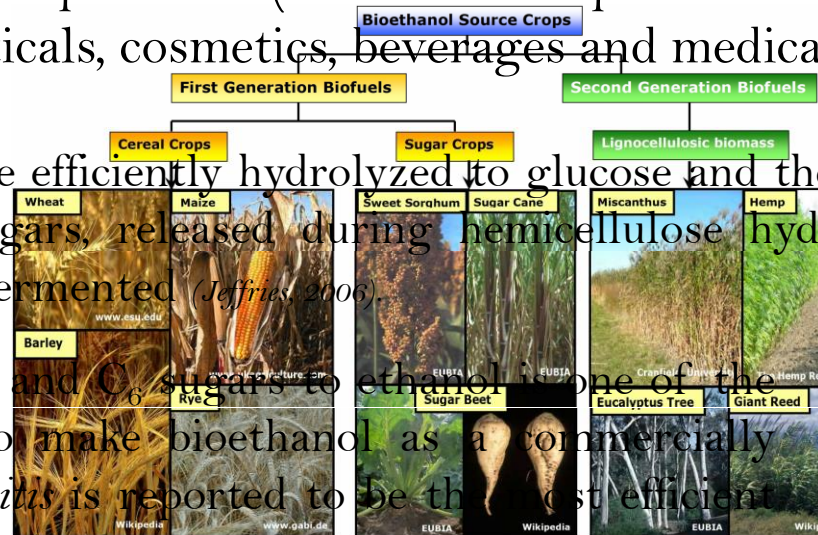


The production of bioethanol from traditional means, or *1st generation bioethanol* is based upon *starch crops* (corn and wheat) and from *sugar crops* (sugar cane and sugar beet)

It could be used as transport fuel (blended with petrol at 5%). A wide range of uses in the pharmaceuticals, cosmetics, beverages and medical sectors

Although cellulose can be efficiently hydrolyzed to glucose and then fermented to ethanol, xylose and other C_5 sugars, released during hemicellulose hydrolysis, are much more difficult to be efficiently fermented (Jeffries, 2006).

Bioconversion of both C_5 and C_6 sugars to ethanol is one of the most important issues to make bioethanol as a commercially viable product. *Pichia stipitis* is reported to be the most efficient and highly productive strain for significant ethanol production from xylose (Cheng et al., 2008).



Chemical composition

Characteristic	Value
TS (%)	90.90 ± 0.04
VS (%TS)	79.54 ± 0.09
Cellulose (%TS)	27.79 ± 2.57
Hemicellulose (%TS)	18.73 ± 2.37
Lignin (%TS)	22.34±0.26
Ash (%TS)	1.09±0.56



Chemical composition after pretreatment

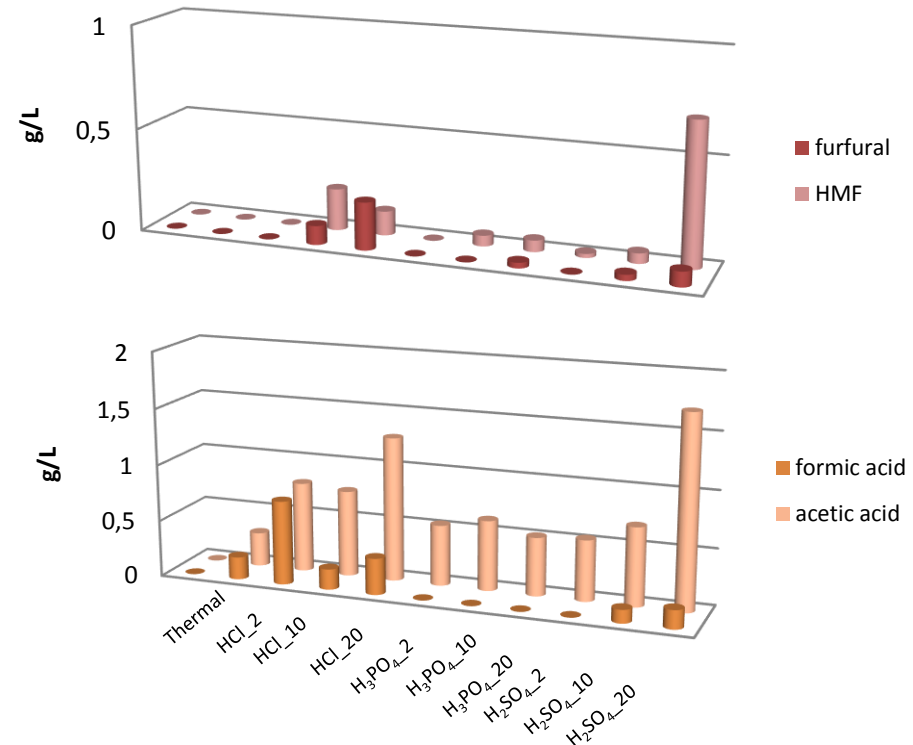
Pretreatment		Cellulose (g/100gTS)	Hemicellulose (g/100gTS)	Lignin (g/100gTS)
no	thermal	28.49 ± 0.21	18.26 ± 0.37	22.11 ± 1.31
H ₂ SO ₄	2 g/100gTS	27.74 ± 1.22	13.41 ± 1.00	20.80 ± 0.35
	10 g/100gTS	29.87 ± 0.27	10.51 ± 0.36	21.36 ± 1.28
	20 g/100gTS	29.09 ± 0.14	7.60 ± 2.80	20.78 ± 0.14
H ₃ PO ₄	2 g/100gTS	26.46 ± 2.11	13.81 ± 2.14	20.55 ± 0.77
	10 g/100gTS	27.22 ± 0.42	11.89 ± 0.62	20.06 ± 0.07
	20 g/100gTS	27.65 ± 0.60	10.65 ± 0.29	19.41 ± 0.35
HCl	2 g/100gTS	27.24 ± 1.97	13.53 ± 0.41	19.11 ± 0.76
	10 g/100gTS	27.59 ± 0.58	6.66 ± 2.36	19.21 ± 1.56
	20 g/100gTS	26.46 ± 0.26	4.32 ± 0.35	18.56 ± 0.56





Chemical composition after pretreatment

Pretreatment		Sugars (g/100gTS)
no	raw	2.71 ± 0.16
	thermal	2.80 ± 0.13
H ₂ SO ₄	2 g/100gTS	3.74 ± 1.22
	10 g/100gTS	8.69 ± 0.12
	20 g/100gTS	13.79 ± 0.12
H ₃ PO ₄	2 g/100gTS	2.78 ± 0.19
	10 g/100gTS	3.48 ± 0.01
	20 g/100gTS	5.30 ± 0.60
HCl	2 g/100gTS	2.87 ± 0.01
	10 g/100gTS	11.36 ± 0.92
	20 g/100gTS	12.68 ± 2.01



✓ Treatment with HCl of 10 and 20g/100gTS and H₂SO₄ at 20g/100gTS, led to higher hemicellulose solubilisation and higher furfural and HMF concentration values

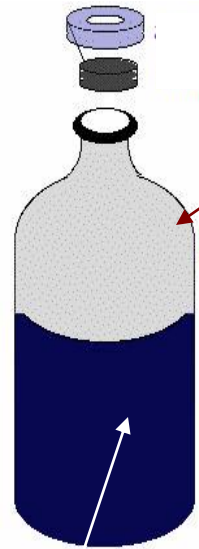
✓ The higher the acid concentration, the higher the HMF and furfural which was produced (Hendriks, and Zeeman, 2009).





Fermentative hydrogen production

160 mL serum vials



Headspace

Inoculum (20%v/v)



Biogas measurement



Hydrogen content

☀ **Inoculum:** Anaerobic sludge from the anaerobic digester of Patras wastewater treatment plant: **boiled for 15min at 100°C**

☀ **Assays:** In 160mL serum bottles, at 35°C: **10mL inoculum + 30mL synthetic medium + 10mL whole pretreated biomass (0.5gTS SS + 10 mL of each chemical agent) → 5% organic load**

☀ Mixture of **Celluclast 1.5L** + **Novozyme** at a ratio of **3:1**, (**30FPU Celluclast/gTS**)

Cellulase from *Trichoderma reesei*, ATCC 26921

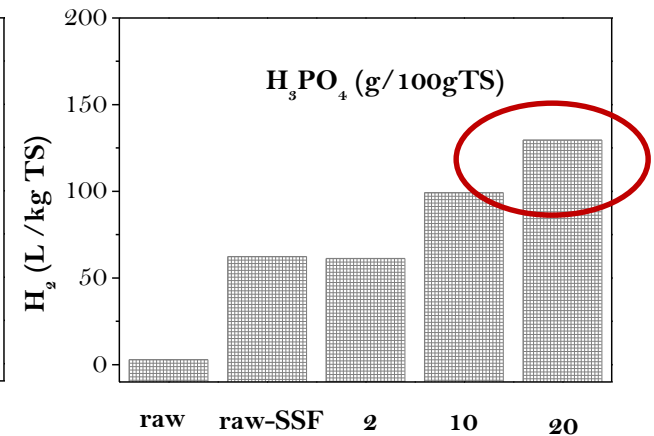
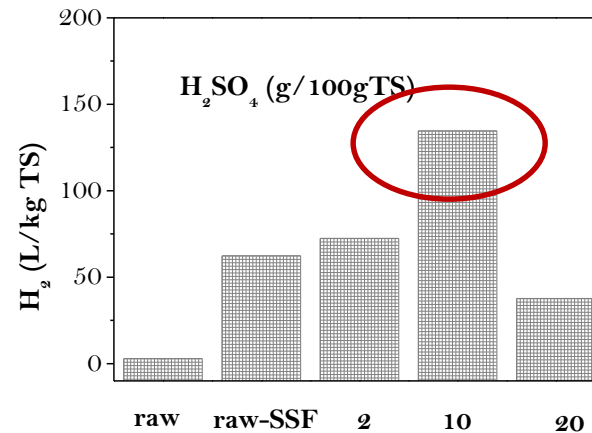
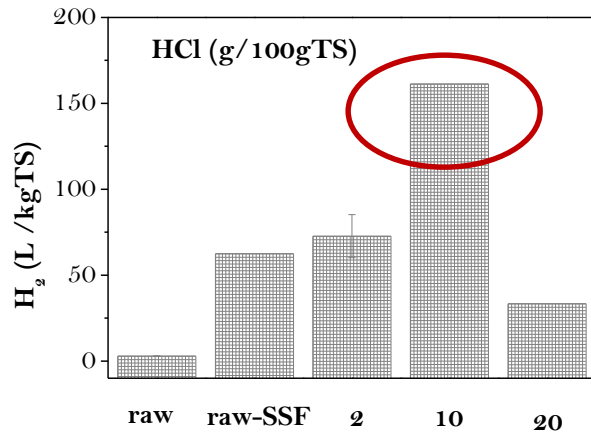
Cellobiase from *Aspergillus niger*

☀ **Agitation at 100rpm at 35°C**





Fermentative hydrogen production

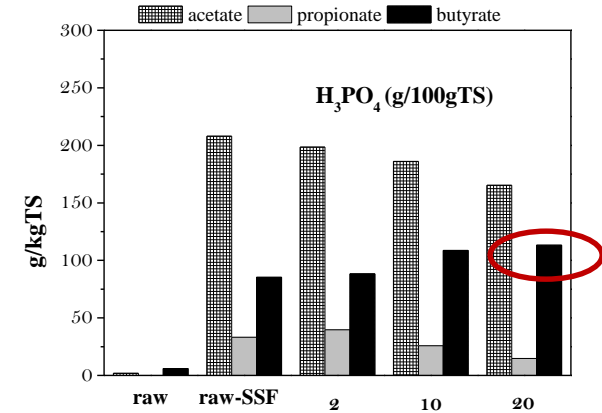
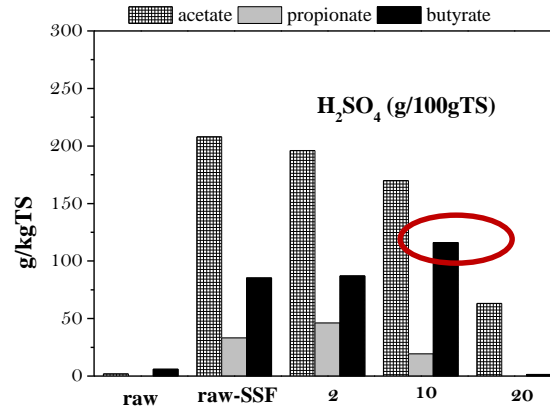
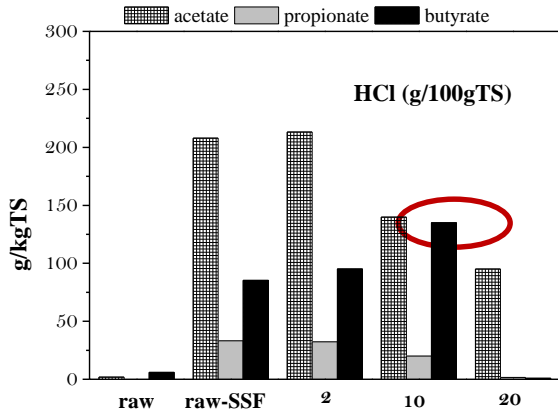


- ✓ Treatment with HCl and H₂SO₄ of 10g/100gTS and H₃PO₄ of 20g/100gTS led to **higher hydrogen yields**.
- ✓ Treatment with HCl 10g/100gTS caused a **159% increase** when compared with the untreated sample (in a SSF concept- **62.4L/kg TS**).
- ✓ Concentration of HCl and H₂SO₄ of 20g/100gTS caused an inhibition to hydrogen production microorganisms.

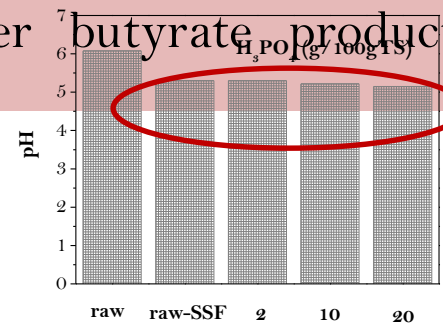
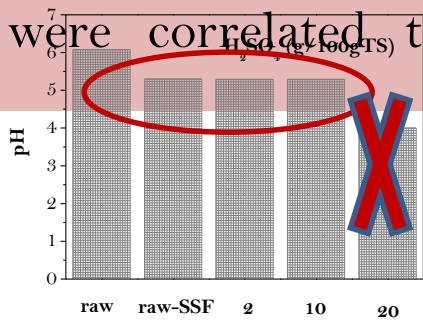
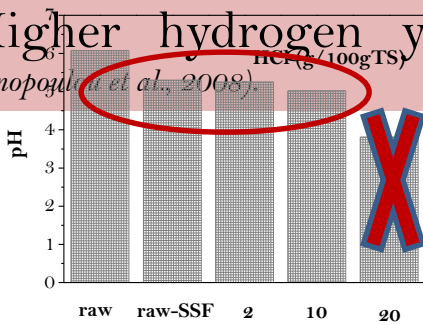




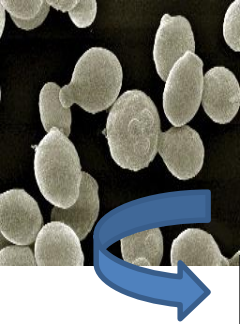
Fermentative hydrogen production



✓ Higher hydrogen yields were correlated to higher butyrate production (Antonopoulos et al., 2008).



Ethanol fermentation experiments



Pichia Stipitis (strain CECT 1922)



- ☀ Solution (g/L): KH_2PO_4 , (1) $\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$, (1) $(\text{NH}_4)_2\text{SO}_4$, (1)
- ☀ C5 and C6 sugars uptake
- ☀ Main metabolic products: Ethanol -xylitol

The whole pretreated biomass (0.75gTS SS + 15 mL of each chemical agent) → 5% organic load

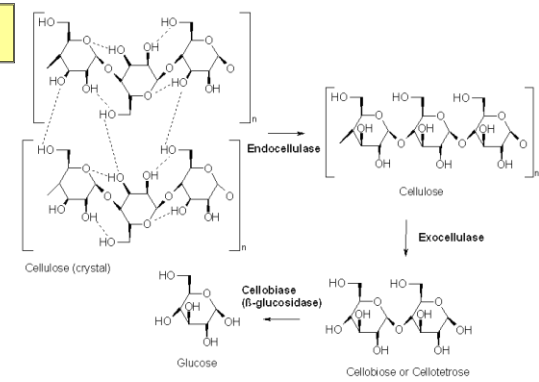
☀ Mixture of **Celluclast 1.5L** + **Novozyme** at a ratio of 3:1, (30FPU Celluclast/gTS)

Cellulase from *Trichoderma reesei*, ATCC 26921

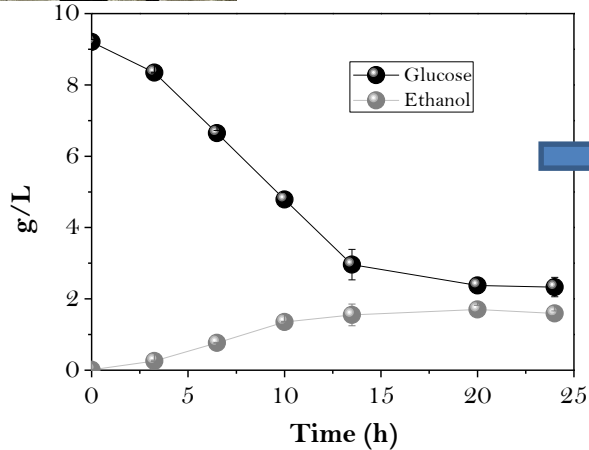
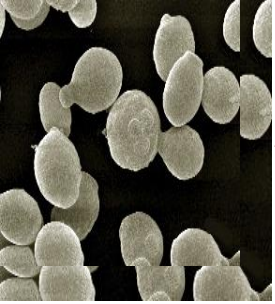
Cellobiase from *Aspergillus niger*

- ☀ Adjustment of initial pH at 5
- ☀ Agitation at 100rpm at 30°C

☀ Fermentation for 48h



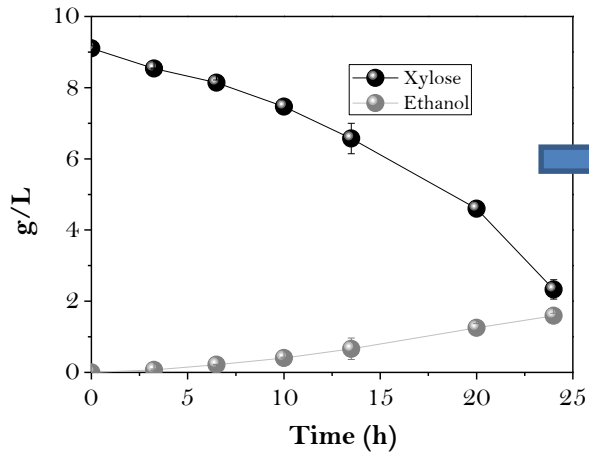
Ethanol fermentation experiments



0.28 g ethanol/g glucose
1.08 mol ethanol / mol glucose



54 % of maximum theoretical



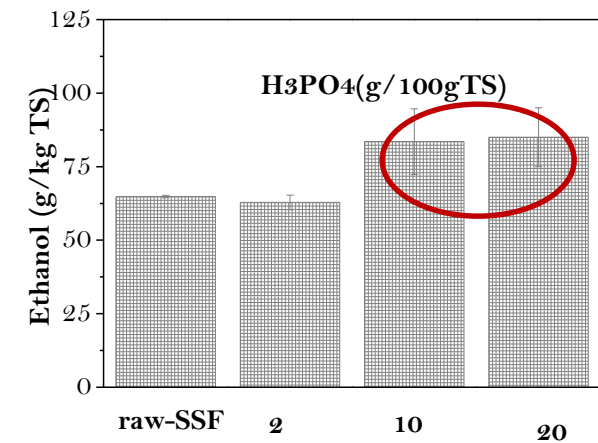
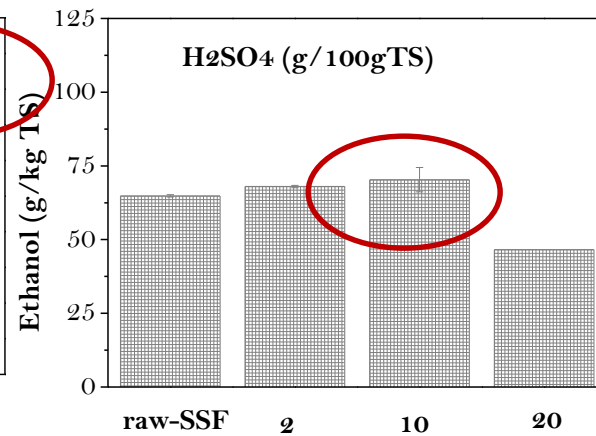
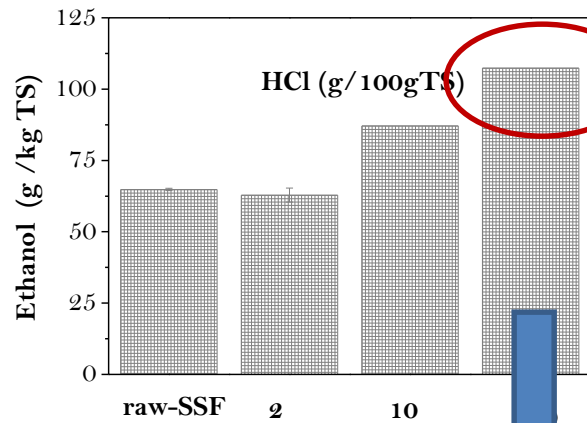
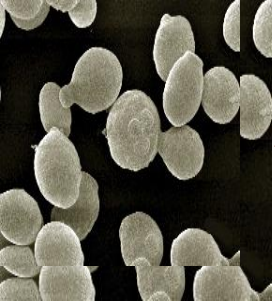
0.28 g ethanol/g xylose
0.91 mol ethanol / mol xylose



55 % of maximum theoretical



Ethanol fermentation experiments



- ✓ Treatment with HCl and H₃PO₄ of 20g/100gTS led to **higher ethanol yields**.
- ✓ Concentration of H₂SO₄ of 20g/100gTS caused an inhibition to *P.stipitis*.

78% of the maximum obtained






Conclusions

- ☀ Acid pretreatment could be used to enhance hydrogen and ethanol production from SS
- ☀ The optimum, for hydrogen production, pretreatment method, was not the optimum for ethanol production, implying that the same pretreatment method is not appropriate for all subsequent bio-conversion processes.
- ☀ Pretreatment with HCl seems to be more effective. HCl at 10g/100gTS led to 161.35 LH₂/kg TS while HCl at 20g/100gTS led to 107 g ethanol/kg TS.
- ☀ Higher hydrogen yields were correlated to higher butyrate production
- ☀ Pretreatment with H₂SO₄ at 20g/100gTS led to higher furfural and HMF concentration and led to lower ethanol and hydrogen production yields.



Thank you very much!



General Secretariat for Research and Technology
“Supporting Postdoctoral Researchers Projects” -
Pretreatment of lignocellulosic wastes for 2nd
generation biofuels (POSTDOC _ PE8(1756)) (post-doc
fellowship of Dr. G. Antonopoulou).